Amendments to the specification:

Kindly replace existing paragraph 144 by the following paragraph:

[0144] The results of the calculation are shown in Table 5. Stream numbers refer to Figure 6.

TABLE 5

Stream	602	605	608	609	612	615	616
Flow (lbmol/h)	329	360	324	36.0	92.5	87.0	5.5
Flow (MMscfd)	3.0	3.3	2.9	0.3	0.8	0.8	0.1
Temp. (°C)	27	18	18	18	49	48	48
Pressure (psia)	365	125	120	20	140	125	50
Component (mol%):							
Helium[-4]	0.8	0.8	0.5	3.0	8.4	7.8	17.8
Nitrogen	1.0	1.1	1.0	1.8	2.3	2.3	2.4
Carbon Dioxide	3.0	3.1	2.5	8.5	20.1	19.3	32.7
Methane	81.6	82.3	82.3	82.9	66.3	67.7	44.6
Ethane	7.0	6.6	7.1	2.3	1.2	1.2	0.3
Propane	4.1	3.8	4.1	0.9	0.4	0.4	0.1
C_4 - C_6	2.3	2.1	2.3	0.04	0.02	0.02	--
Water	0.2	0.2	0.2	0.6	1.3	1.3	2.2
Hydrogen Sulfide (ppm)	<1	<1	<1	<1	<1	<1	<1

Kindly replace existing paragraph 146 by the following paragraph:

[0146] A computer calculation was performed to demonstrate the invention as it applies to treatment of fuel gas, according to the embodiment of Figure 7. The fuel gas stream 702 was assumed to be taken off as shown in that figure at the front of the gas processing train and to be of the same mole percent composition as in Example 5, that is:

Helium	0.8%
Nitrogen	1.0%

Carbon dioxide	3.0%
Methane	81.6%
Ethane	7.0%
Propane	4.1%
C_4-C_6	2.3%
Water	0.2%
Hydrogen sulfide	0.1 ppm.

The results of the calculation are shown in Table 6. Stream numbers refer to Figure 7.

TABLE 6

Stream	702	705	708	709	712
Flow (lbmol/h)	416	416	324	92.4	92.4
Flow (MMscfd)	3.8	3.8	3.0	0.8	0.8
Temp. (°C)	27	27	24	25	330
Pressure (psia)	365	365	360	20	375
Component (mol%):					
Helium[-4]	0.8	0.8	0.1	3.3	3.3
Nitrogen	1.0	1.0	0.8	1.7	1.7
Carbon Dioxide	3.0	3.0	1.4	8.7	8.7
Methane	81.6	81.6	81.4	82.3	82.3
Ethane	7.0	7.0	8.3	2.5	2.4
Propane	4.1	4.1	5.0	0.9	0.9
C_4 - C_6	2.3	2.3	2.9	0.05	0.05
Water	0.2	0.2	0.1	0.6	0.6
Hydrogen Sulfide (ppm)	<1	<1	<1	<1	<1